PRODUCED WATER SOCIETY SEMINAR 2020

Membrane Distillation (MD) : A novel approach to produced water desalination in Heavy Oil Assets

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Thermal Oil Recovery : Heavy Oil Fields

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Produced Water Geochemistry

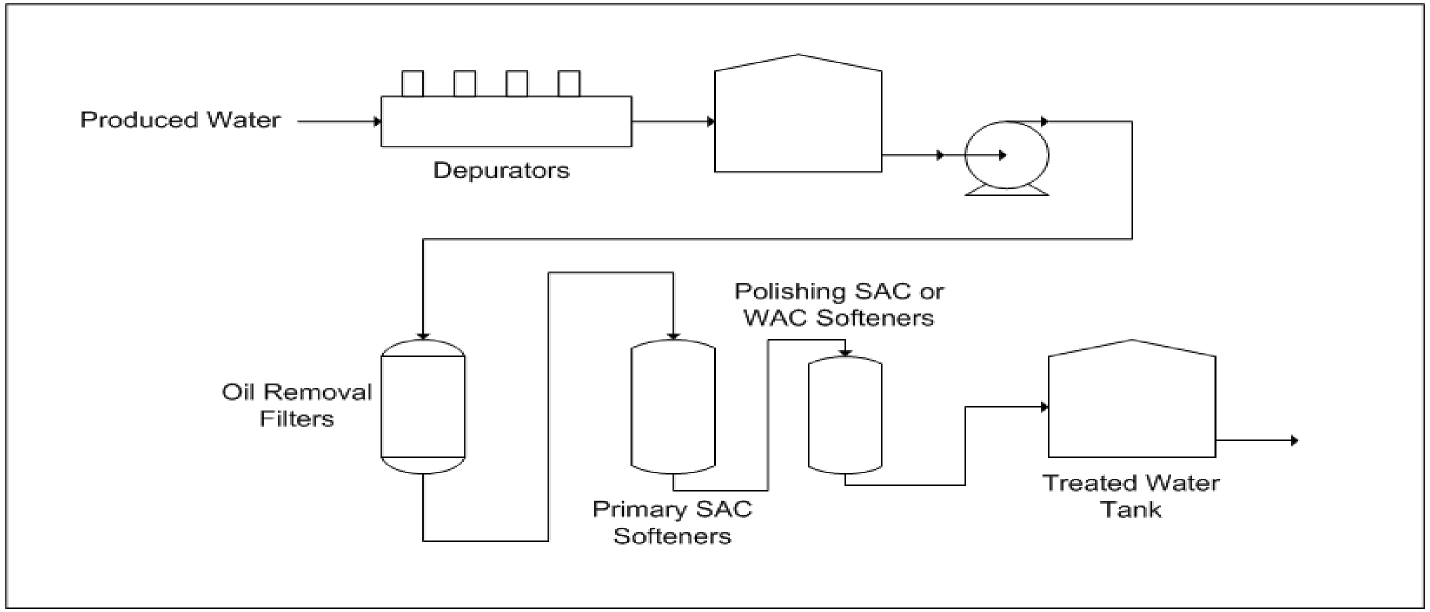
- **Associated with the geology of the reservoir**
  - Carbonate Reservoir
  - Sandstone Reservoir
- **High hardness or high silica**
- **High temperature**

	California	Canada	Middle East
Hardness (as CaCO3)	150-200	10-140	1000-9000
HCO3- (mg/L)	500-1500	200-400	500-1000
SiO2 (mg/L)	175-350	250-350	10-40
TDS (mg/L)	5000-7500	1000-6000	7,000-35,000
Temp (F)	160 - 180	170 - 190	170-200

Desalination Drivers

- **Environmental & Regulatory**
    - Reduce reliance on disposal injection
    - Increase reuse of produced water (internal + export) including beneficial reuse
    - Minimize use of freshwater, esp. 3rd party supplies
- **Operations**
    - Reduce CAPEX and OPEX for water plants
    - Consolidate or eliminate treatment stages
    - Improve treatment performance (e.g., efficiency, separation, permeate recovery, reliability, sanding, tolerance to oil upsets, fouling, and scaling)
    - Reduce chemical use and waste generation (esp. liquids/brine)
    - Decrease energy consumption and GHG emissions
    - Replace existing systems at end of life and/or instead of repair
- **Technology Investment**
    - Optimize technology investment budgets and timing
- **Organizational Capability**
    - Optimize BU resources, develop OC in water treatment technologies
- **Asset Development**
    - Meet future production water handling needs (capacity)
    - Extend life of asset by removing reservoir capacity constraints

Steamflood Water Treatment Requirements



- **Deoiling**
- **Softening**
  - SAC/SAC Softeners
  - SAC/WAC Softeners
  - Usually applied to low TDS waters
  - Silica is not removed but it does form scales in Once Through Steam Generators
- **Usually no desalination required**

Desalination vs Softening for Steamflood : Drivers

- **Silica removal is not addressed in softening**
- **Softening costs may be too high if water has high hardness and TDS**
  - Salt consumption during softener regeneration
  - Caustic/acid consumption is high
  - Logistics of bulk chemicals transport
  - Independent studies have shown that OPEX is significantly high
- **High temperature of produced water can be of value**
  - High temperature RO membranes (has its own challenges and is evolving)
  - Thermal Desalination (subject of this presentation)
    - Normally considered for high TDS waters but may find value in these conditions
- **Quality of product water is very high with very low TDS**
  - Steam quality can be very high (only limited by design of the OTSGs)
  - Target Quality : 80% - 85%

Comparison of matured Thermal Desalination technologies with RO

- MVC
- **Pros**
- Robust
- High recovery
- Wide range feed water quality including TDS
- Can handle wide temperature range
- Insensitive to impurities (e.g. oil)
- Minimum pre treatment

- RO
- **Pros**
- No exotic materials
- Can be inside a building
- Less capex
- Simple process

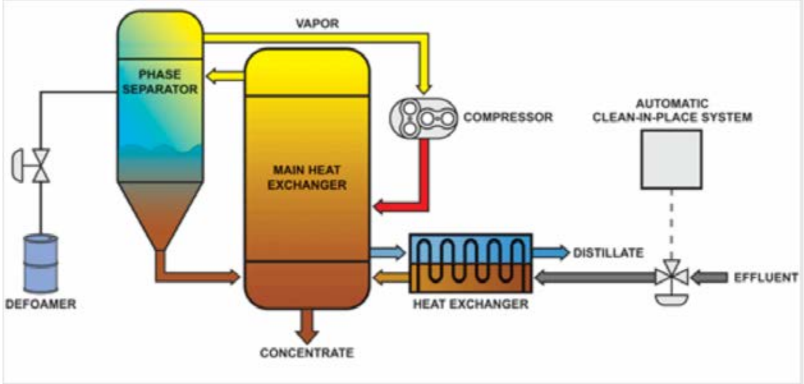
Comparison of matured Thermal Desalination technologies with RO

- MVC
- **Cons**
- Exotic materials
- Bulky equipment
- High capex
- High power consumption
- Complex process

- RO
- **Cons**
- Extensive pretreatment
- Susceptible to impurities
- Low recovery
- unproven > 113 F (HTRO research)
- TDS limitations on feed
- Water quality of permeate not as good as distilled water

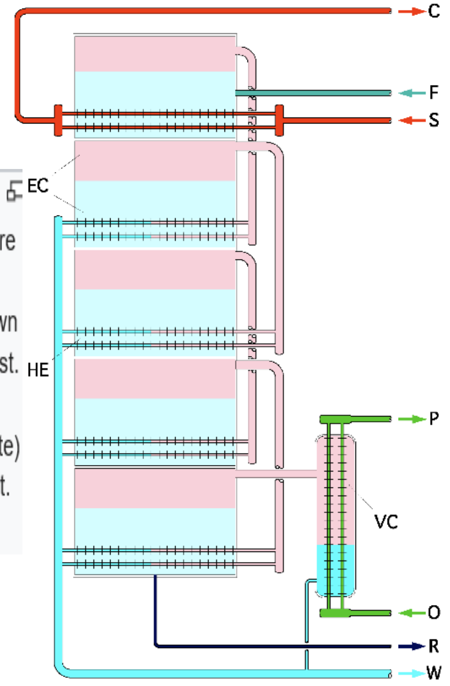
Thermal Desalination Technologies

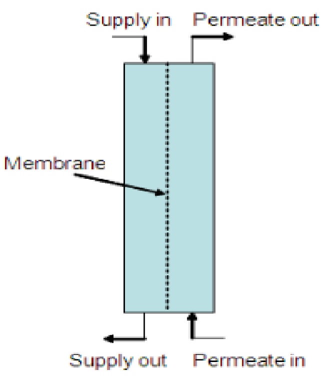
Mechanical Vapor Compression



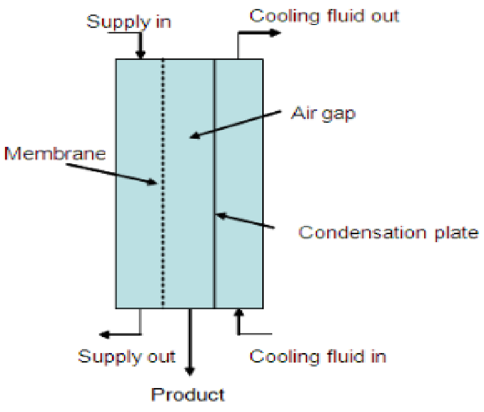
Multiple Effect Distillation

Schematic of a multiple effect desalination plant. The first stage is at the top. Pink areas are vapor, lighter blue areas are liquid feed water. Stronger turquoise is condensate. It is not shown how feed water enters other stages than the first. F - feed water in. S - heating steam in. C - heating steam out. W - Fresh water (condensate) out. R - brine out. O - coolant in. P - coolant out. VC is the last-stage cooler.

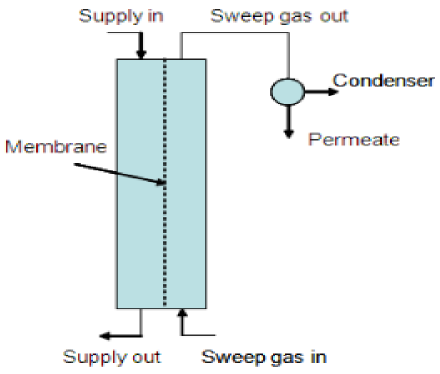




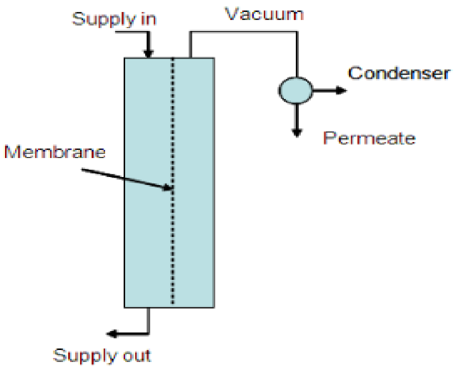
DCMD configuration



AGMD configuration



SGMD configuration



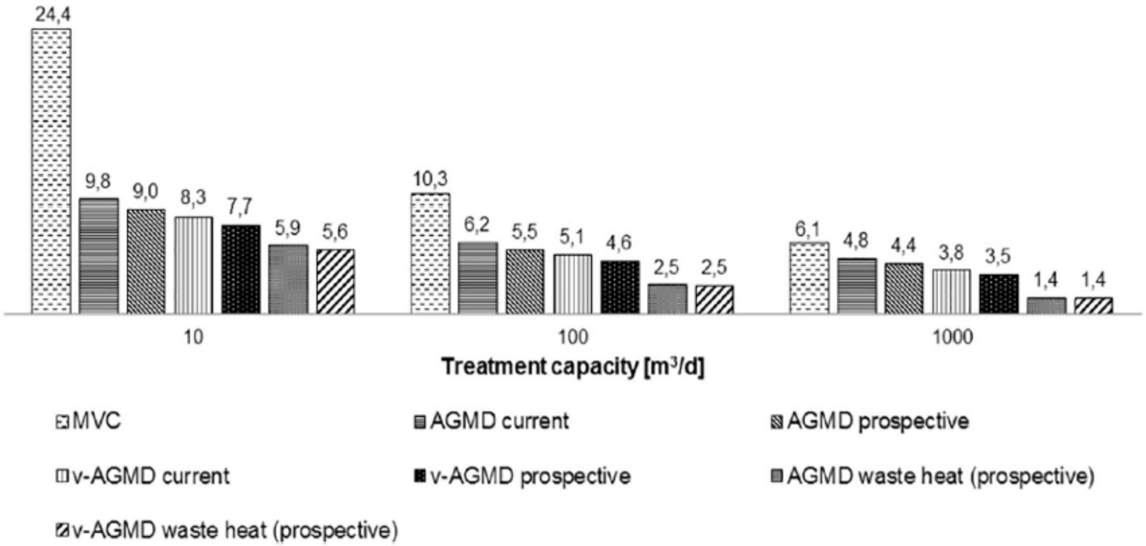
VMD configuration

Membrane Distillation (MD)

DCMD – Direct Contact Membrane Distillation; AGMD – Air Gap Membrane Distillation; SGMD – Sweep Gas Membrane Distillation; VMD – Vacuum Membrane Distillation

Membrane Distillation : Advantages

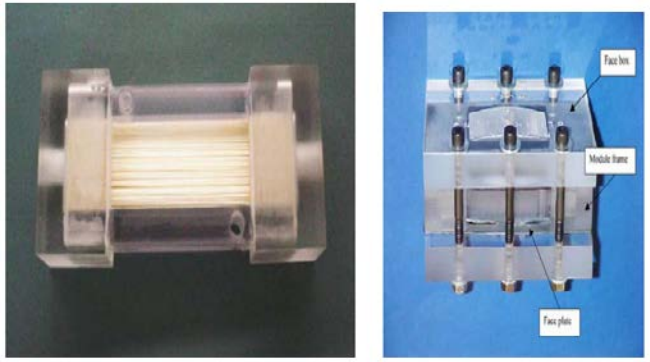
- **Lower operating temperature than conventional distillation – improved integrity of equipment**
- **Lower operating pressure than RO - lower fouling propensity**
- **Polymeric material of construction – lower Capex**
- **Limited pretreatment**
- **Almost 100% rejection of nonvolatile solutes**
- **No effect of osmotic pressure**
- **Can remove 99.8% boron & silica without pH adjustment**



Schwantes et al :
Desalination 428
(2018) 50 - 68

Membrane Distillation : Experimental Work

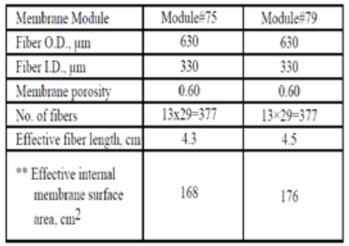
- Carried out at Professor Kam Sirkar's Lab in NJIT
- Each module picture frame contains porous polypropylene hollow fibers having on their outside surface a highly porous plasma polymerized fluorosilicone coating.
- Hot produced water was pumped on the shell side in cross flow over the hollow fibers and the cold distillate solution was pumped through the lumen side of the hollow fibers by two peristaltic pumps (Masterflex, Cole-Parmer, Vernon Hills, IL).
- The feed produced water was obtained from a 55 gal drum sent by Chevron Inc. (Richmond, CA).
- A sample of this water was heated in a constant temperature bath (A81, HAAKE, Germany).



(a) (b)

Figure 2. Photographs showing (a) rectangular cross flow test module with out face plates etc. (b) rectangular cross flow test module with face boxes, face plates and assembly (Made at NJIT).

Table 1. Characteristics of DCMD modules used in produced water treatment



Membrane Module	Module#75	Module#79
Fiber O.D., μm	630	630
Fiber I.D., μm	330	330
Membrane porosity	0.60	0.60
No. of fibers	13x29=377	13×29=377
Effective fiber length, cm	4.3	4.5
** Effective internal membrane surface area, cm^2	168	176

*Membrane picture frame supplied by Applied Membrane Technology, Inc, Minnetonka, MN; flow distributors and cover plate fabricated at NJIT.
**Based on fiber internal diameter (I.D.)

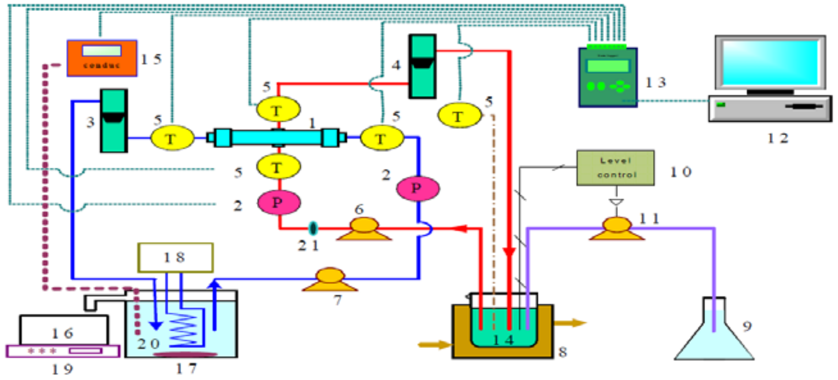
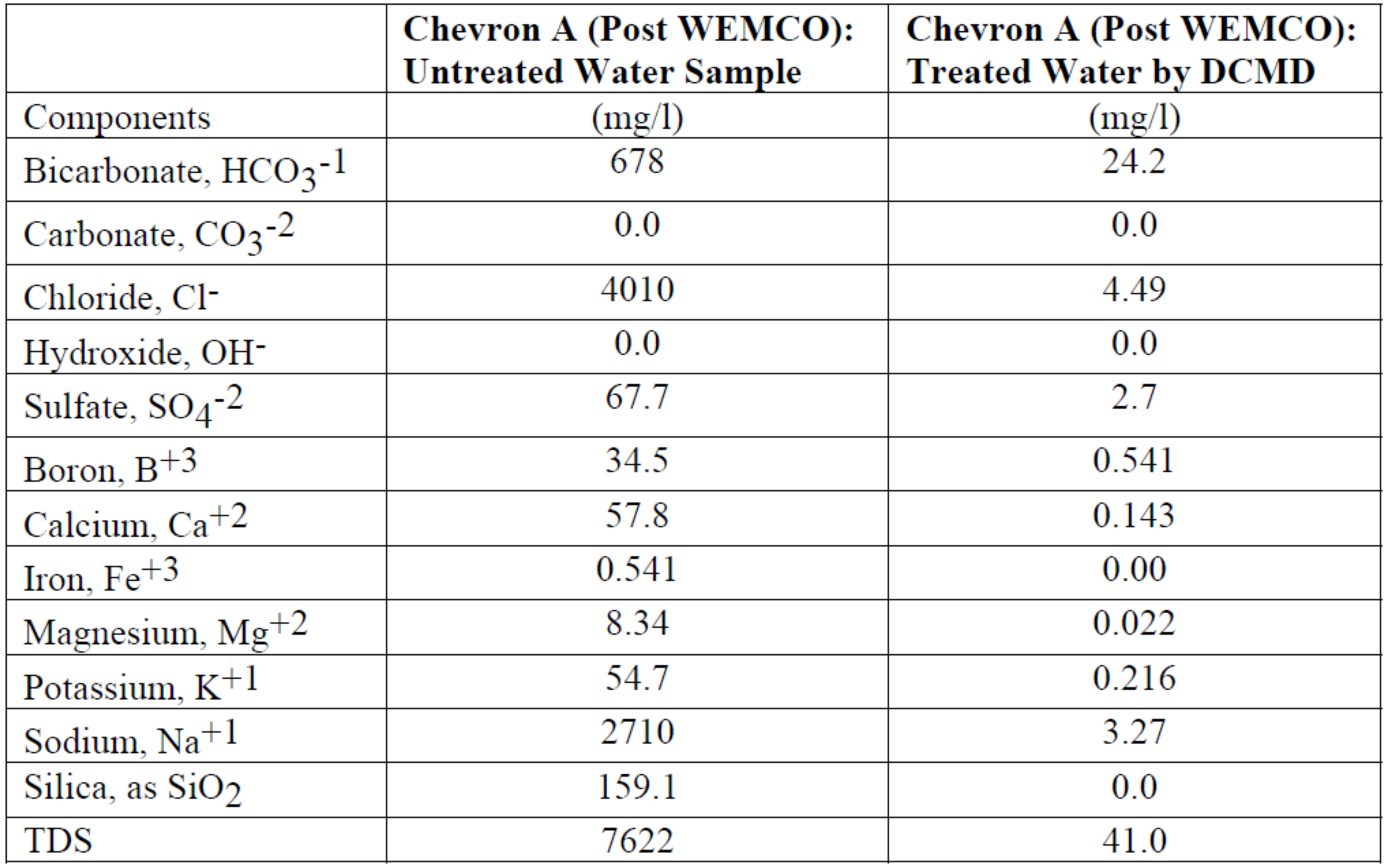


Figure 1. Low temperature DCMD setup:
1.Membrane module; 2. Pressure indicator; 3. Distillate flowmeter; 4. Urine flowmeter; 5. Thermocouple; 6. Hot urine pump; 7. Distillate pump; 8. Constant temperature bath; 9. Make-up water reservoir; 10. Level controller; 11. Make-up pump; 12. Computer; 13. Data logger; 14. Hot brine beaker; 15. Conductivity transmitter; 16. Distillate overflow reservoir; 17. Magnetic stirrer; 18. Chiller; 19. Weight balance; 20. Cold distillate beaker; 21. Filter holder.

DCMD: Results

- **Four different waters were tested. Results of two water samples shown below. One was high silica. The other has both high silica and hardness**

Table 5. Water chemistries for untreated/treated Chevron A (Post-Wemco)



	Chevron A (Post WEMCO): Untreated Water Sample	**Chevron A (Post WEMCO): Treated Water by DCMD**
Components	(mg/l)	(mg/l)
Bicarbonate, HCO_3^{-1}	678	24.2
Carbonate, CO_3^{-2}	0.0	0.0
Chloride, Cl^-	4010	4.49
Hydroxide, OH^-	0.0	0.0
Sulfate, SO_4^{-2}	67.7	2.7
Boron, B^{+3}	34.5	0.541
Calcium, Ca^{+2}	57.8	0.143
Iron, Fe^{+3}	0.541	0.00
Magnesium, Mg^{+2}	8.34	0.022
Potassium, K^{+1}	54.7	0.216
Sodium, Na^{+1}	2710	3.27
Silica, as SiO_2	159.1	0.0
TDS	7622	41.0

Ref: DOI: 10.1021/ie4015809

DCMD: Results Contd.

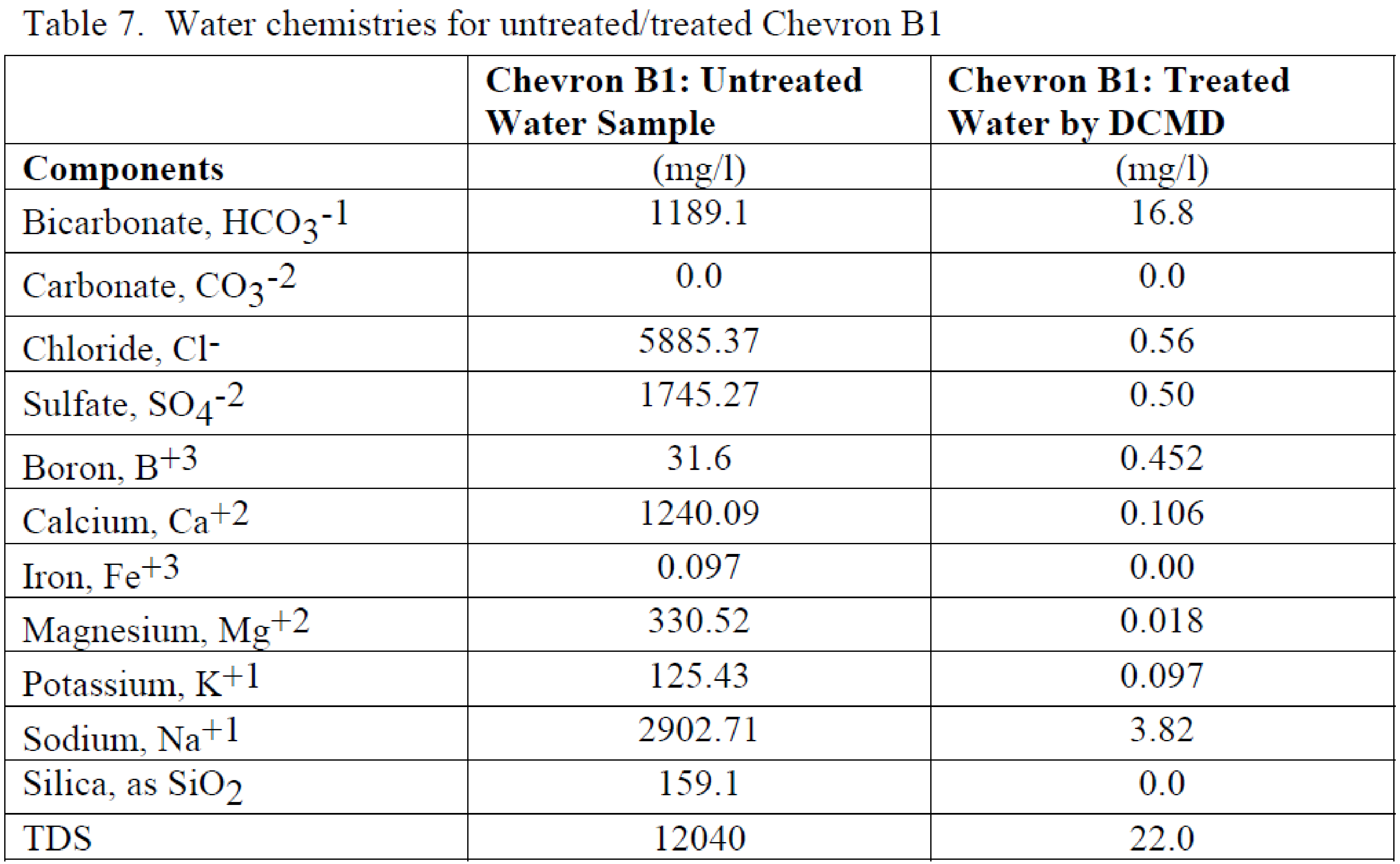


Table 7. Water chemistries for untreated/treated Chevron B1

	Chevron B1: Untreated Water Sample	**Chevron B1: Treated Water by DCMD**
Components	(mg/l)	(mg/l)
Bicarbonate, HCO_3^{-1}	1189.1	16.8
Carbonate, CO_3^{-2}	0.0	0.0
Chloride, Cl^-	5885.37	0.56
Sulfate, SO_4^{-2}	1745.27	0.50
Boron, B^{+3}	31.6	0.452
Calcium, Ca^{+2}	1240.09	0.106
Iron, Fe^{+3}	0.097	0.00
Magnesium, Mg^{+2}	330.52	0.018
Potassium, K^{+1}	125.43	0.097
Sodium, Na^{+1}	2902.71	3.82
Silica, as SiO_2	159.1	0.0
TDS	12040	22.0

Ref: DOI: 10.1021/ie4015809

DCMD: Results Contd.

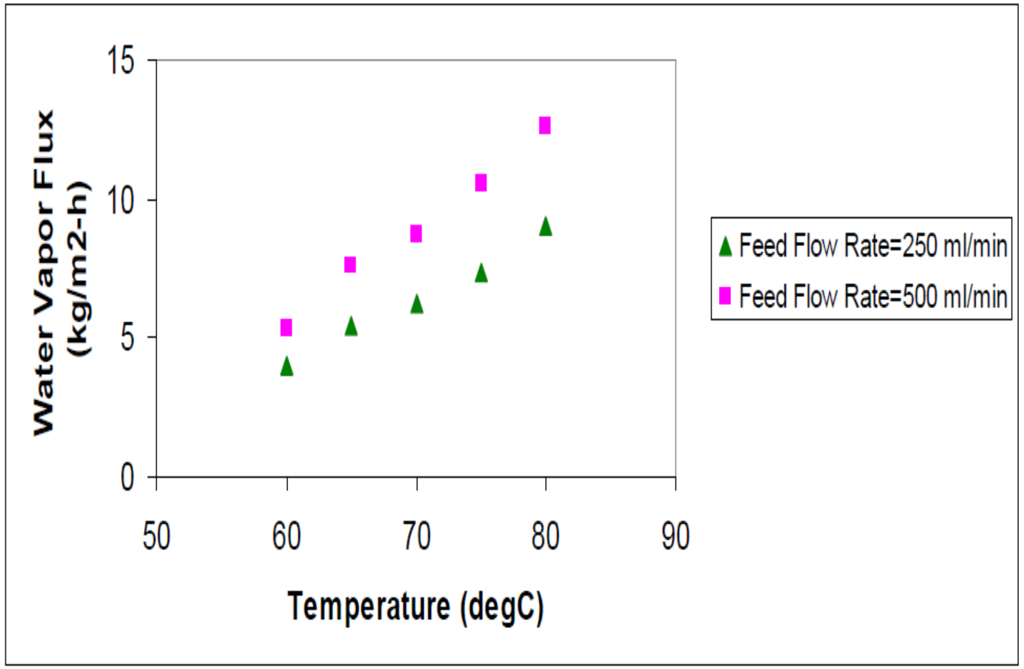


Figure 6. Variation of water vapor flux in DCMD with temperature for Chevron A (Post-Wemco) produced water in rectangular cross flow module #79.

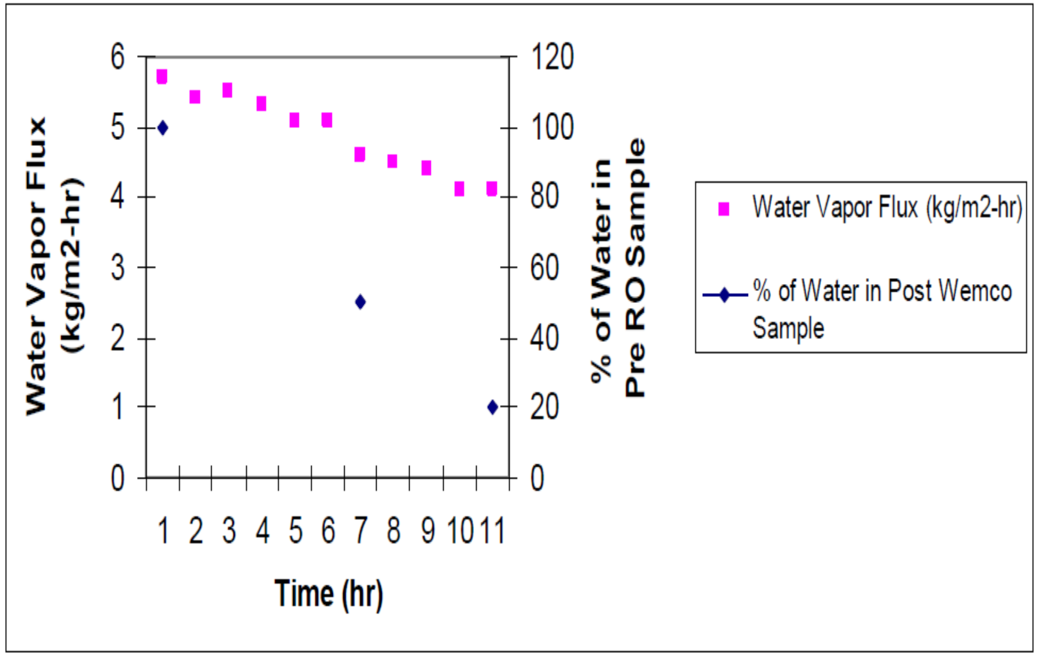


Figure 7. Variation of water vapor flux with time varying concentration of Chevron A (Post-Wemco) produced water at 70° C in rectangular cross flow module #75 during batch recirculation-based feed concentration.

Ref: DOI: 10.1021/ie4015809

DCMD: Results Contd.

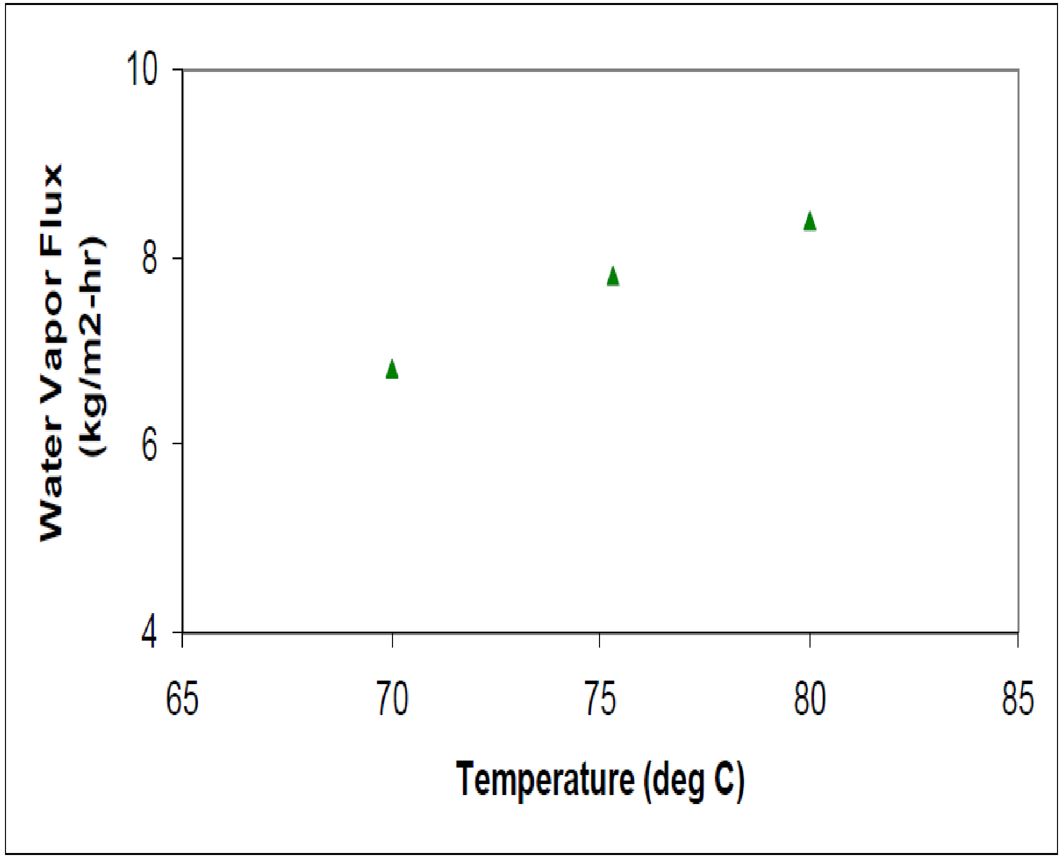


Figure 8. Variation of water vapor flux in DCMD with temperature for Chevron B1 produced water in rectangular cross flow module#75.

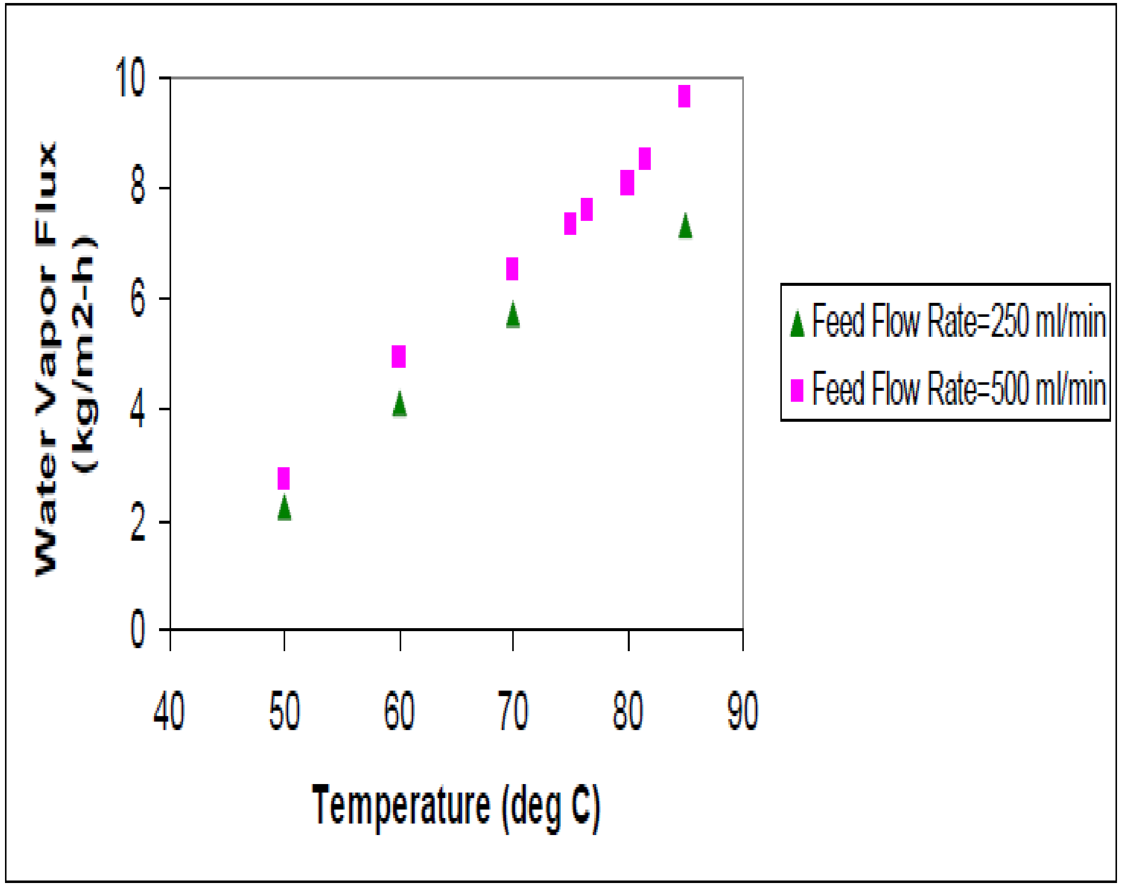


Figure 5. Variation of water vapor flux in DCMD with temperature for Chevron A (Pre-RO) produced water in rectangular cross flow module #75 at two different feed flow rates.

Ref: DOI: 10.1021/ie4015809

DCMD: Results Contd.

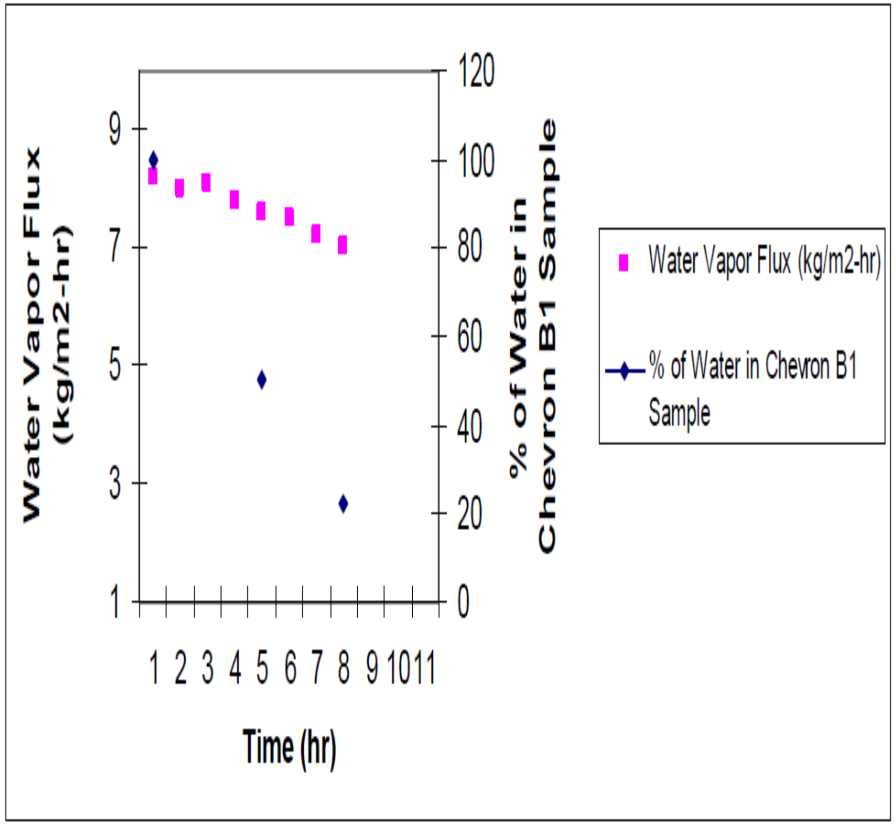


Figure 9. Variation of water vapor flux in DCMD with varying concentration of Chevron B1 at 80°C in rectangular cross flow module #75 during batch recirculation-based feed concentration.

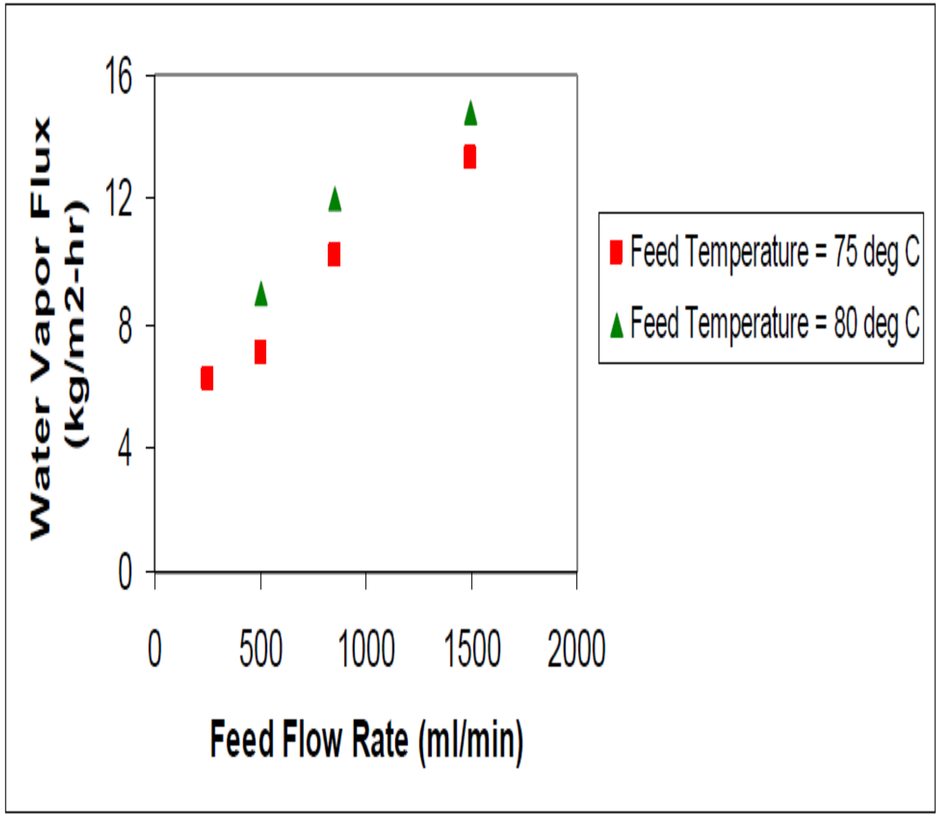


Figure 10. Variation of water vapor flux in DCMD with varying flow rate of Chevron B2 produced water in rectangular cross flow module #75.

Ref: DOI: 10.1021/ie4015809

Conclusions

- **For DCMD Studies, it was concluded that:**
  - DCMD process could be successfully employed to treat different kinds of produced water. The TDS value was very low in the distilled water
  - Water recovery from different produced waters was ~80% by the DCMD process operated in batch recirculation mode when the process was stopped
  - The amount of scaling salt, sodium chloride and silica was almost negligible in the water recovered by distillation; it may be reused for steam generation and a variety of applications. Probably a minor ion exchange polishing will be needed

Conclusions

- **For DCMD Studies, it was concluded that:**
  - At a higher feed flow rate, water vapor flux achieved at 80_0C was 15 kg/m2-hr; at an even higher feed flow rate it may be increased to ~ 20 kg/m2-hr.
  - The novel coated membranes (plasma polymerized fluorosilicone coating) and the hollow fiber cross flow module design are responsible for the observed performances
  - Previous pilots with this geometry provided a GOR of nearly 6. Therefore more studies with this module will be carried out
  - The heat recovery from the hot distillate using heat recovery heat exchangers will be needed in the pilot design

Thanks for your attention !!

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